

# Integrated Modeling of Carbon Management Technologies for Electric Power Systems

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# Some Questions to be Addressed

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- What carbon management technologies may be used in a particular application (e.g., existing vs. new plants)?
- What are the key parameters that affect the performance, emissions, and cost of a given option?
- How do the alternative options compare in terms of performance, reliability, and cost?
- What are the uncertainties and technological risks of different carbon management options?
- What are the priorities and benefits of R&D to reduce key uncertainties in new process designs?

# Scope and Objectives

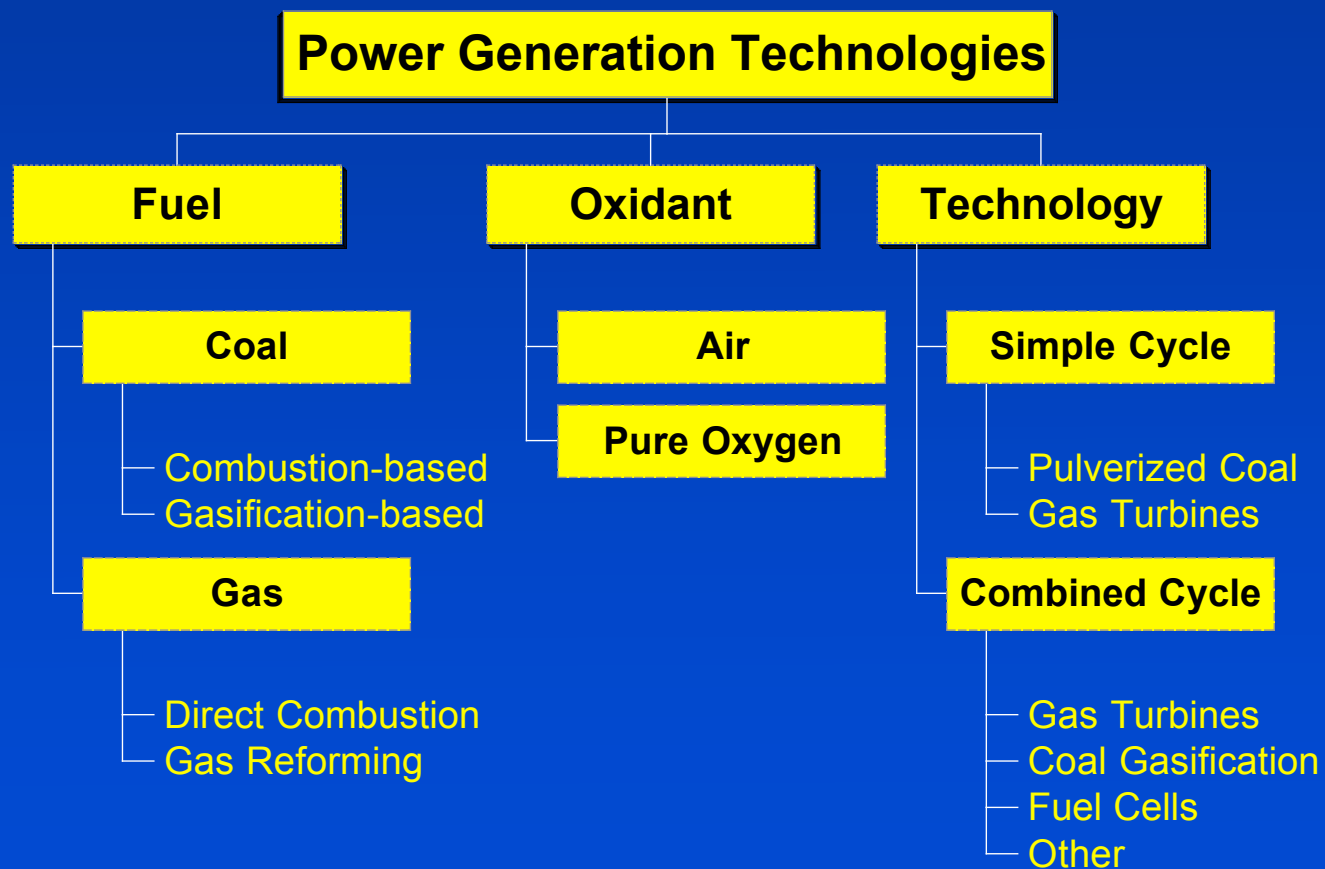
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- Identify potential options for power generation with carbon capture and sequestration, suitable for, (a) existing plants, and (b) new plants
- Develop a model to quantify performance, emissions, and cost of alternative options, and their dependency on key plant and technology design parameters, operating parameters, and carbon management methods
- Characterize uncertainty in key parameters of the carbon management system
- Integrate carbon management technologies with other plant environmental control systems
- Conduct case studies to illustrate model applications

# Current Applications

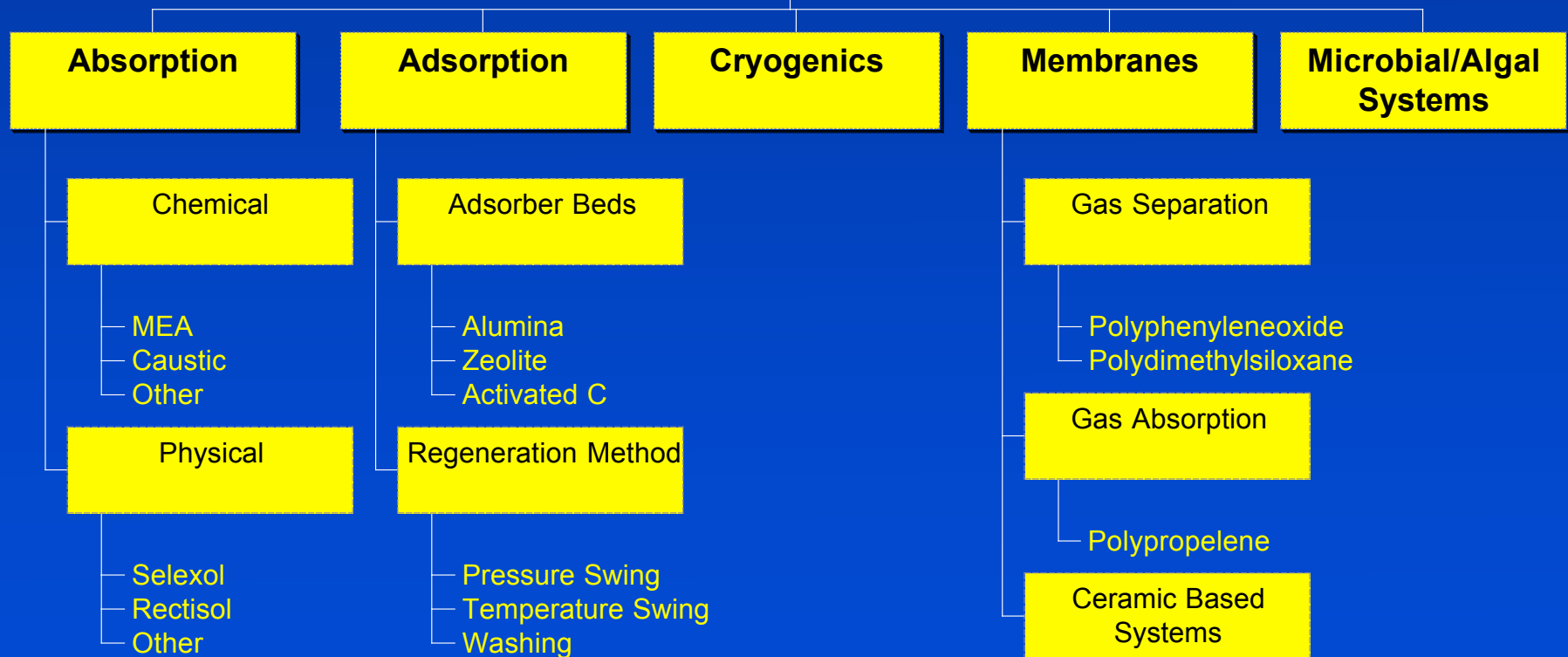
- **Enhanced oil recovery (EOR)**
  - Dow MEA (Some plants in TX and NM, now shut down)
  - Common in 1970s and 1980s (100-1200 tons CO<sub>2</sub>/d)
- **Fertilizer industry**
  - H<sub>2</sub> and CO<sub>2</sub> separation ⇒ Urea production
  - Dow MEA (Indo Gulf Fertilizer Co.) - 150 tons CO<sub>2</sub>/d
- **Carbonation of brine (soda ash)**
  - Kerr-McGee MEA (North American Chemical Co., operational since 1978) - 800 tons CO<sub>2</sub>/d
- **Food-grade**
  - Fluor Daniel / Dow MEA (Northeast Energy Associates, MA) - 320 tons CO<sub>2</sub>/d
- **Commercial CO<sub>2</sub> capture and sequestration facility**
  - Injection into deep saline aquifer (Sleipner West gas field, Norway, installed in 1996) - ~3000 tons CO<sub>2</sub>/d

# Power Generation Options Using Fossil Fuels

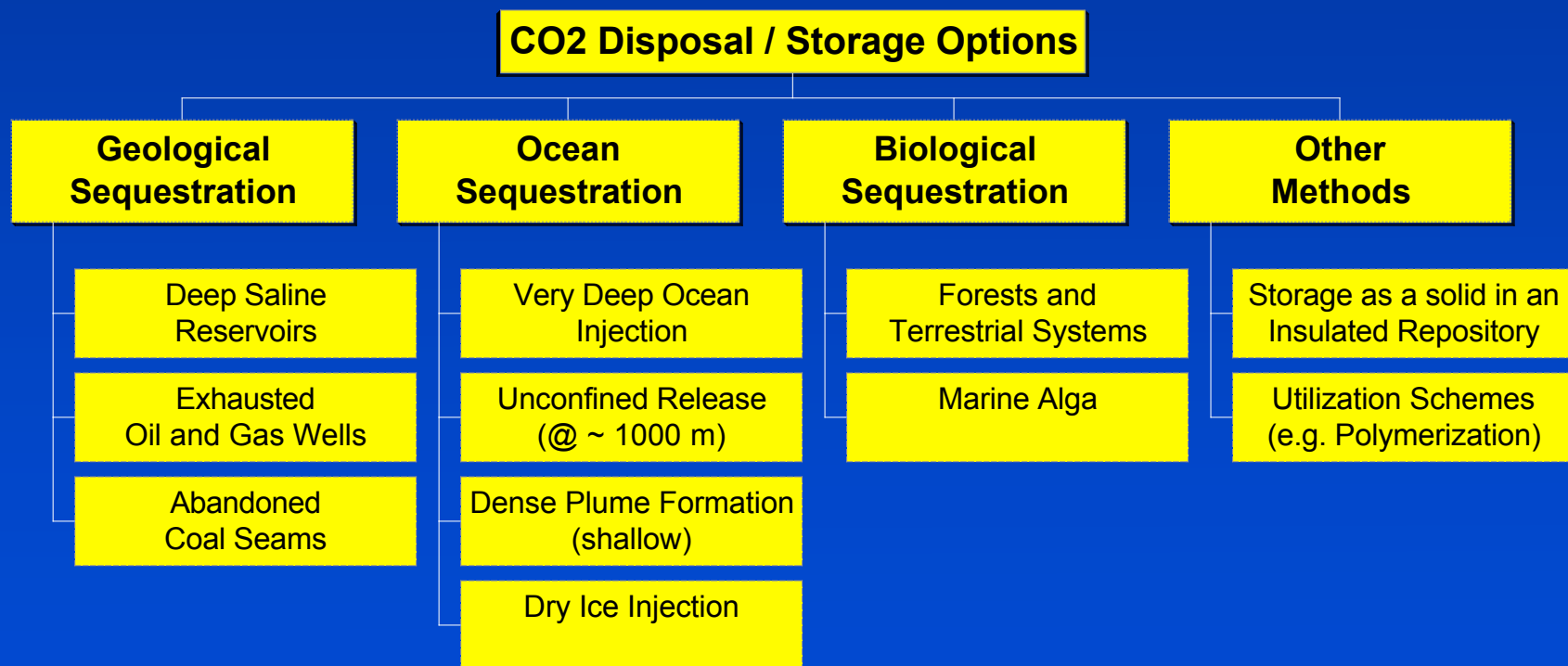


# CO<sub>2</sub> Capture Technologies

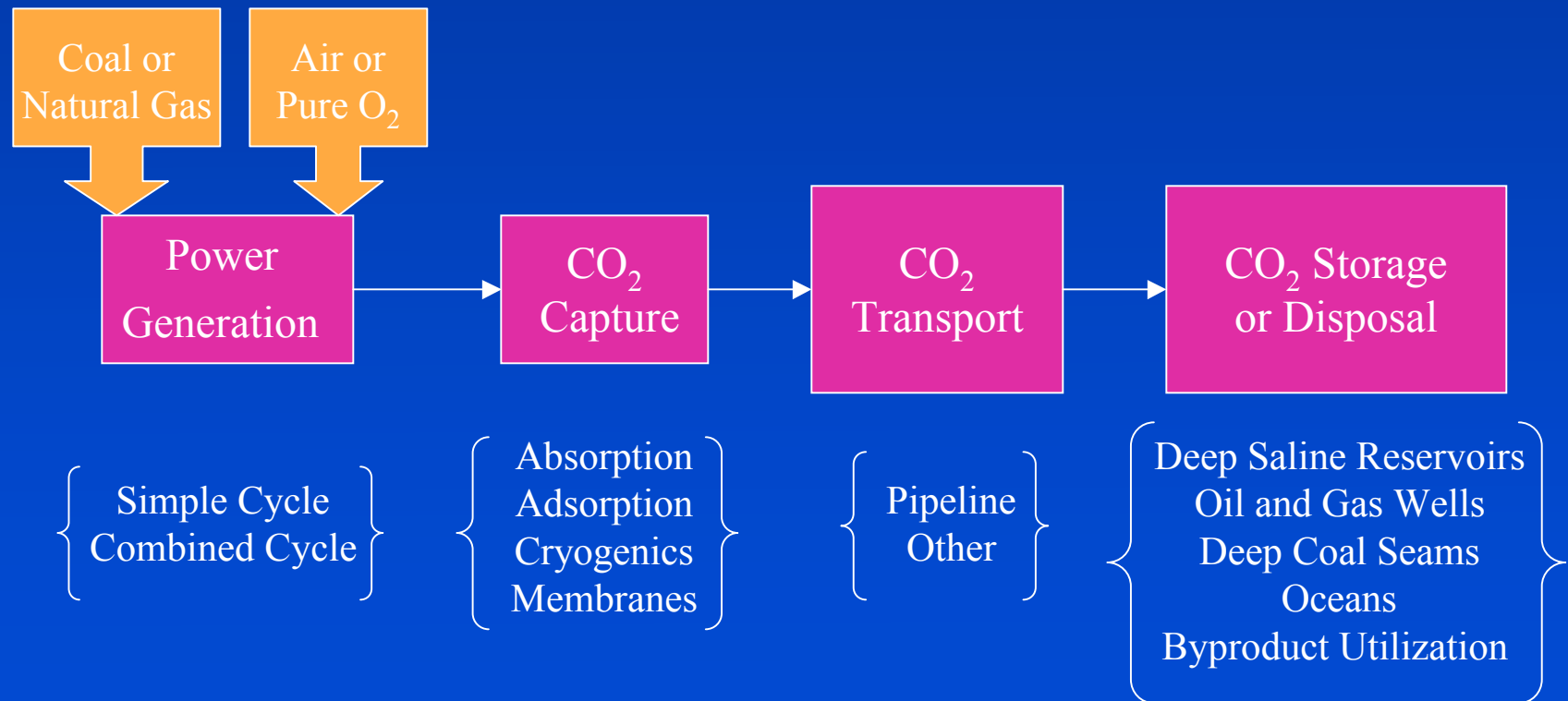
## CO<sub>2</sub> Separation and Capture



# CO<sub>2</sub> Sequestration Options



# Modeling Framework for Carbon Management Options





# Energy Considerations

**Total Energy Required**

**Process Heat**

~ 60-80% cost of separation & capture

**Capture Process**

**Compression**

**Transport**

**Storage/Disposal**

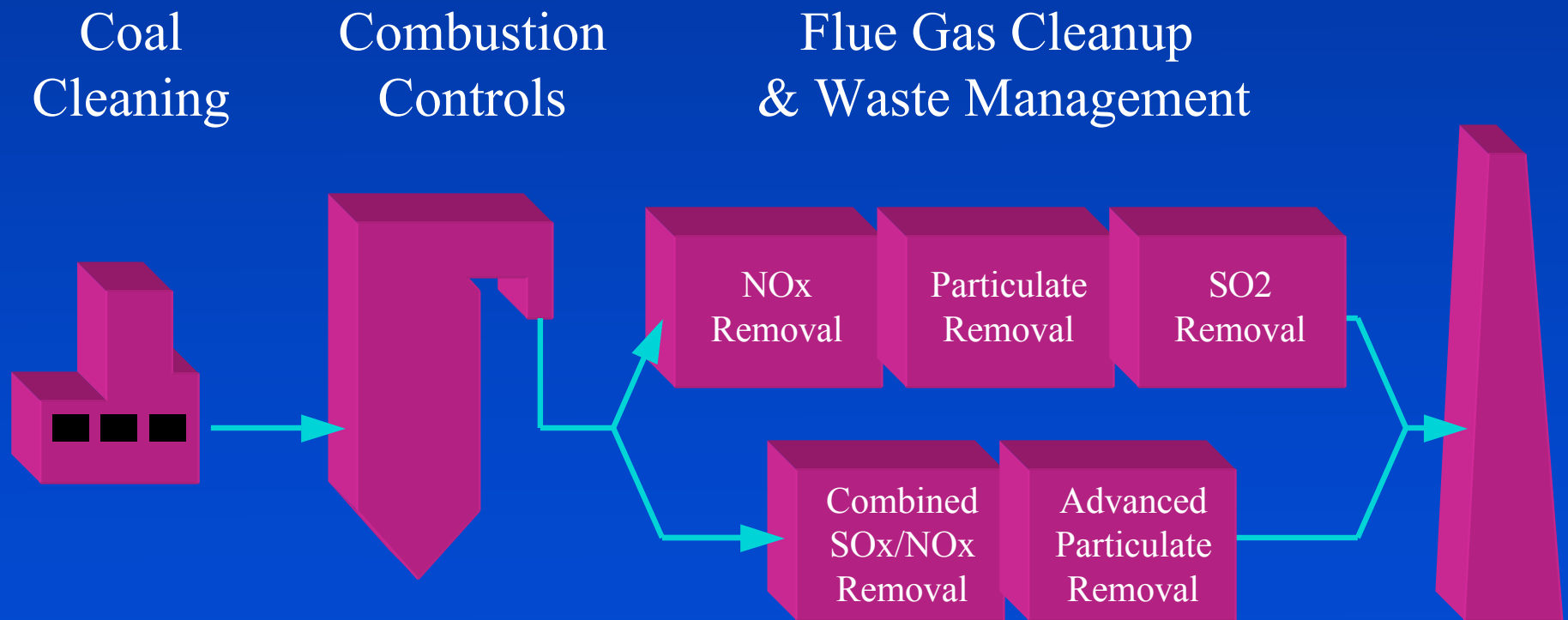
- Gas Stream Flow and Composition
- Choice of CO<sub>2</sub> Capture Technology
  - Desired CO<sub>2</sub> Capture Efficiency
  - Process Parameters
  - Desired CO<sub>2</sub> Product Specifications
  - Mode of Transport
  - Transportation Distance
  - Choice of Disposal Method

# Current Status

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- Developed preliminary models (performance, emissions, and cost) for several CO<sub>2</sub> capture options, CO<sub>2</sub> transport options, and CO<sub>2</sub> storage options
- Initial focus on modeling of current commercial technologies (amine scrubbing systems) for combustion-based power systems
- Integrated the new CO<sub>2</sub> module with the IECM combustion-based power plant model developed for the USDOE

# Integrated Environmental Control Model (IECM)



# Objectives

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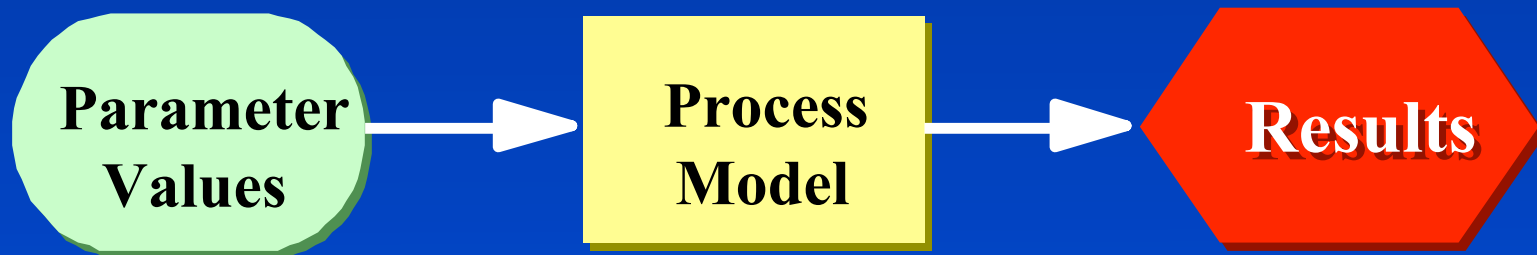
- Develop a comprehensive modeling framework to estimate the performance, environmental emissions, and cost of coal-based power generation technologies
- Develop a method for comparing alternative options on a systematic basis, including the effects of uncertainty

# Probabilistic Software Capability

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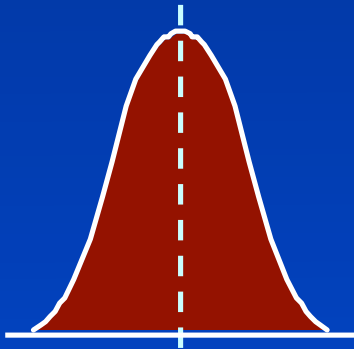
- Allows you to specify parameter values as distribution functions, as well as conventional deterministic (point) estimates
- Allows you to explicitly quantify the effects of uncertainty in performance, emissions, and cost, yielding confidence intervals for uncertain results

# Conventional Process Modeling (Deterministic Simulation)

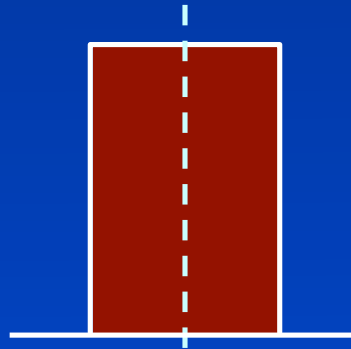


# Parameter Uncertainty Distributions

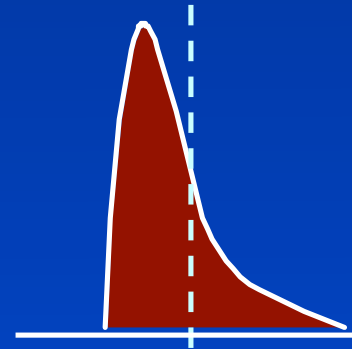
**NORMAL**



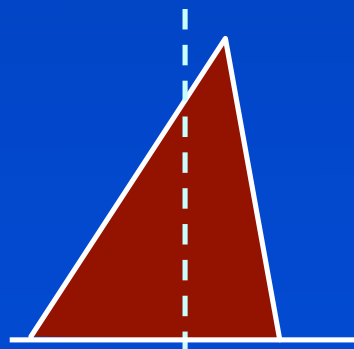
**UNIFORM**



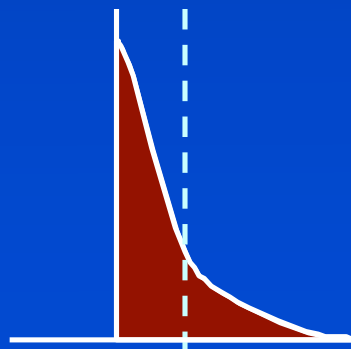
**LOGNORMAL**



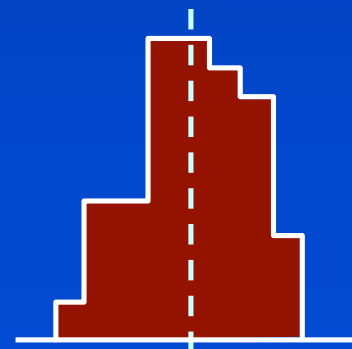
**TRIANGULAR**



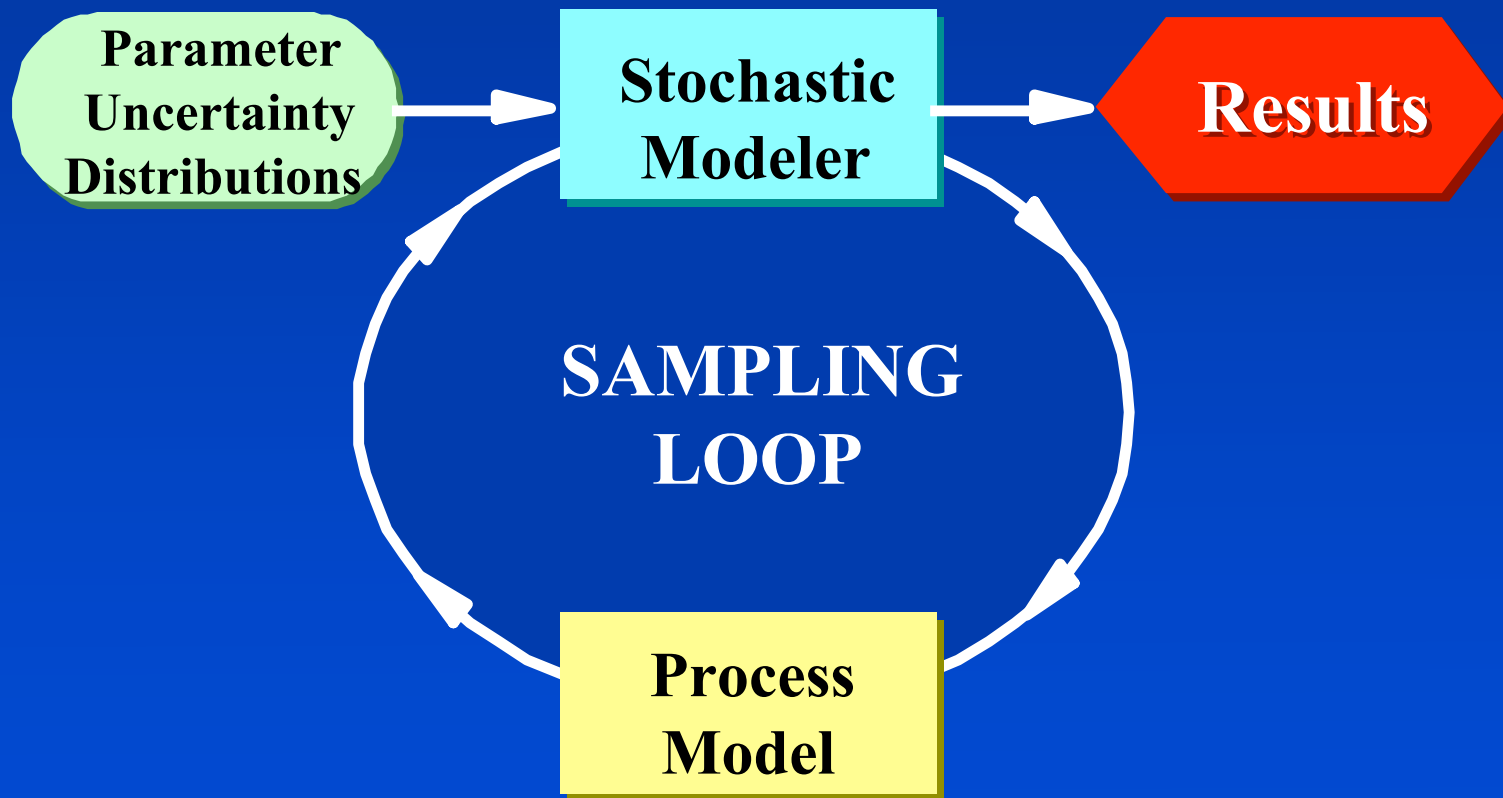
**BETA**



**FRACTILE**



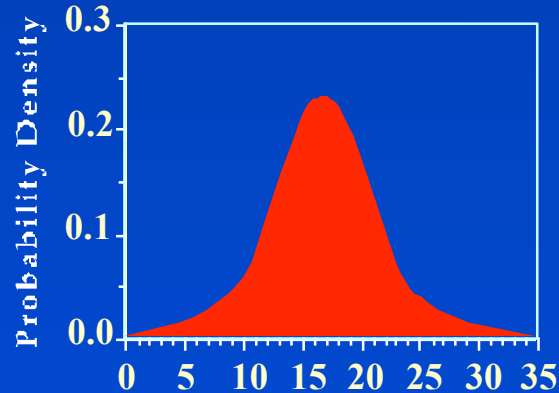
# Stochastic Simulation





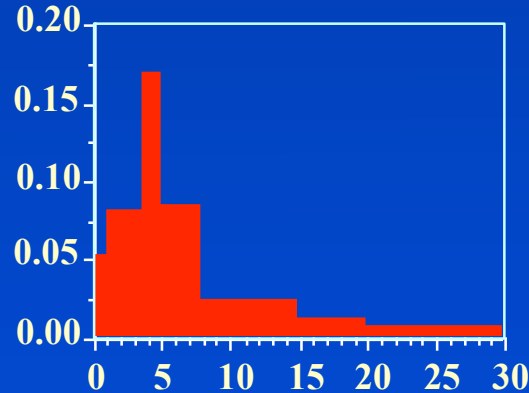
# Expert Judgments on Key Model Parameters

**Sorbent  
Sulfur  
Loading**



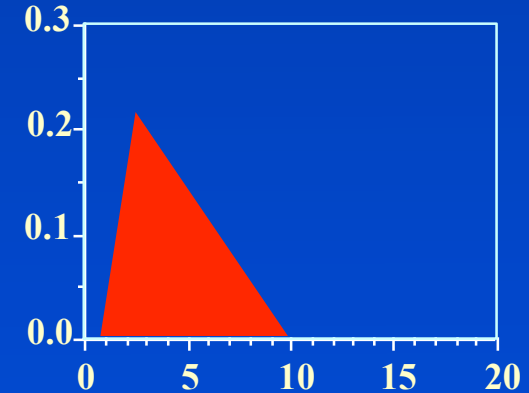
Sorbent Sulfur Loading, wt-%

**Gasifier  
Fines  
Carryover**



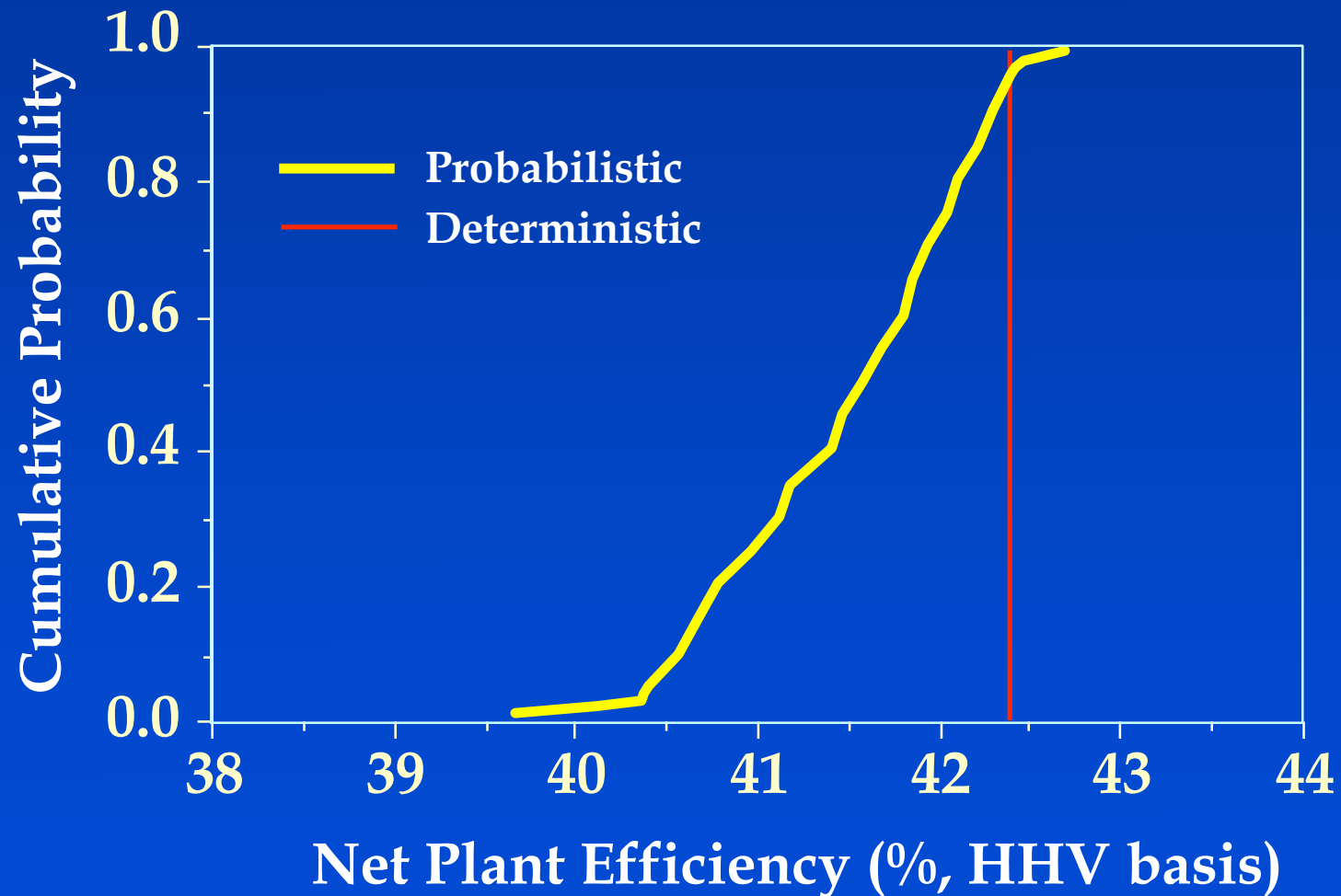
Fines Carryover, % of coal feed

**Carbon  
Retention in  
Bottom Ash**

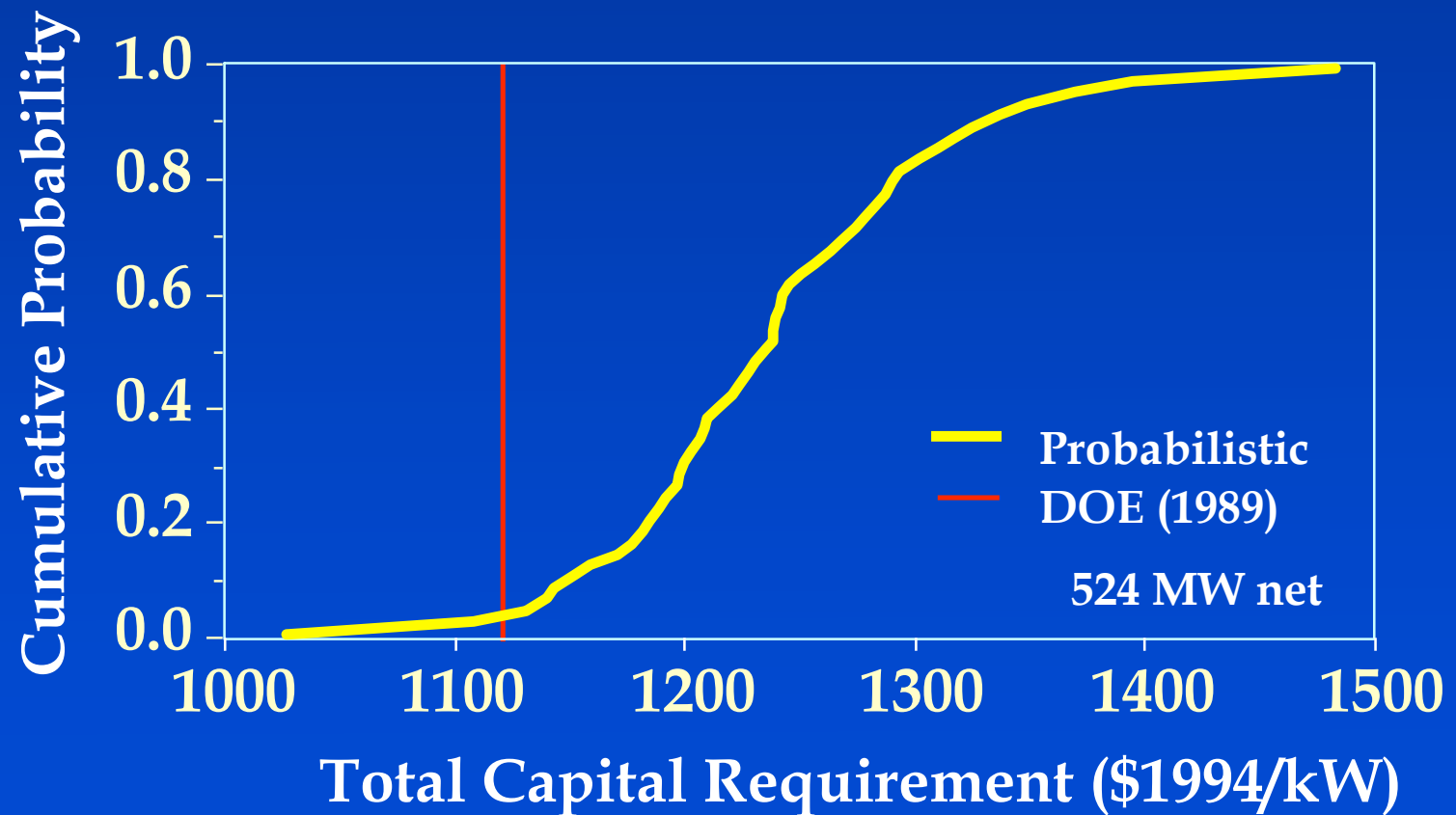


Carbon Retention in Bottom Ash  
% of coal feed carbon

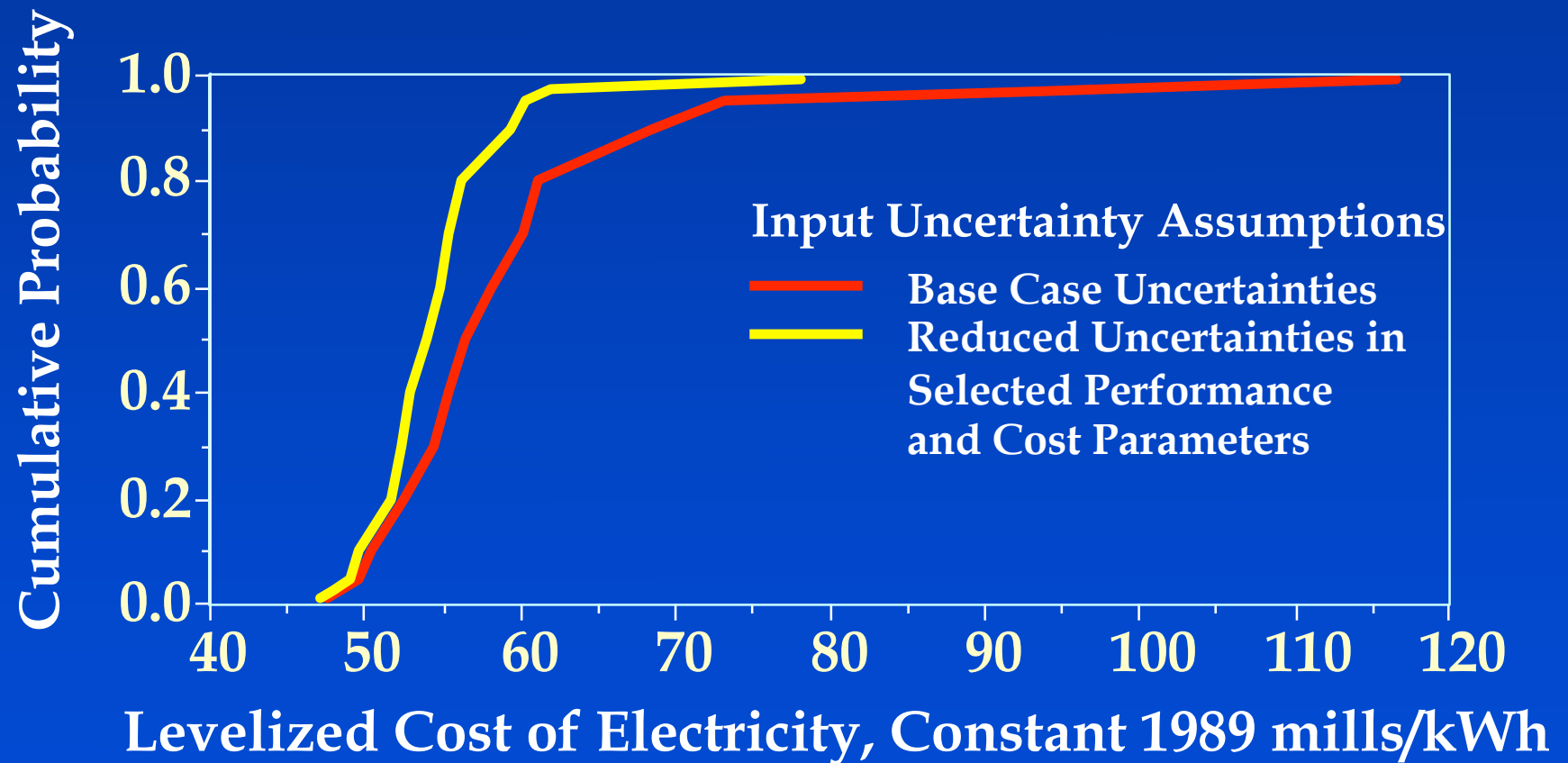
# Calculated Plant Efficiency



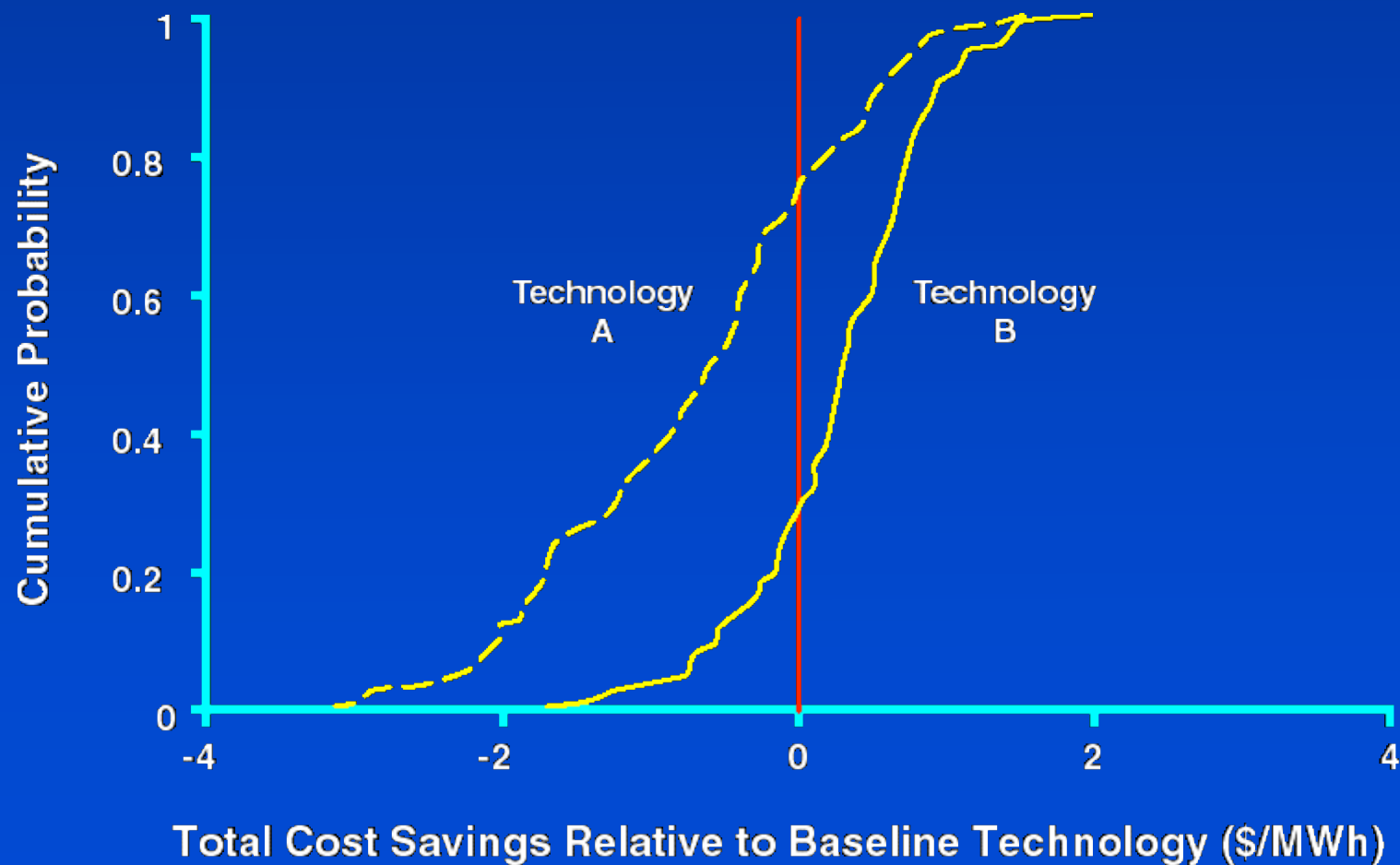
# Total Plant Capital Cost



# Value of Targeted Research



# Probabilistic Comparison of Competing Technologies



# IECM Software Package

## Fuel Properties

Heating Value  
Composition  
Delivered Cost

## Plant Design

Furnace Type  
Emission Controls  
Solid Waste Mgmt  
Chemical Inputs

## Cost Data

O&M Costs  
Capital Costs  
Financial Factors

Power  
Plant  
Model

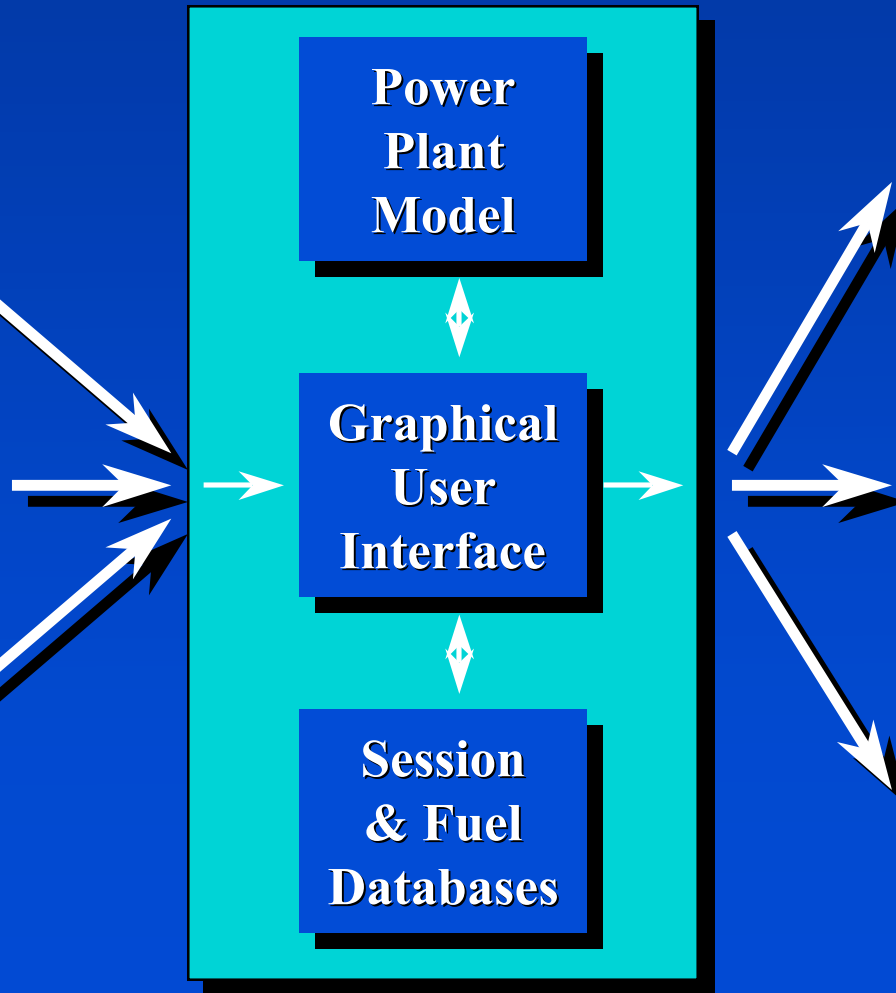
Graphical  
User  
Interface

Session  
& Fuel  
Databases

Plant & Process  
Performance

Environmental  
Emissions

Plant & Process  
Costs



# The IECM is Available for Downloading

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- **Web Access:**

- <ftp://ftp.netl.doe.gov/pub/IECM>

# Preliminary IECM User Group

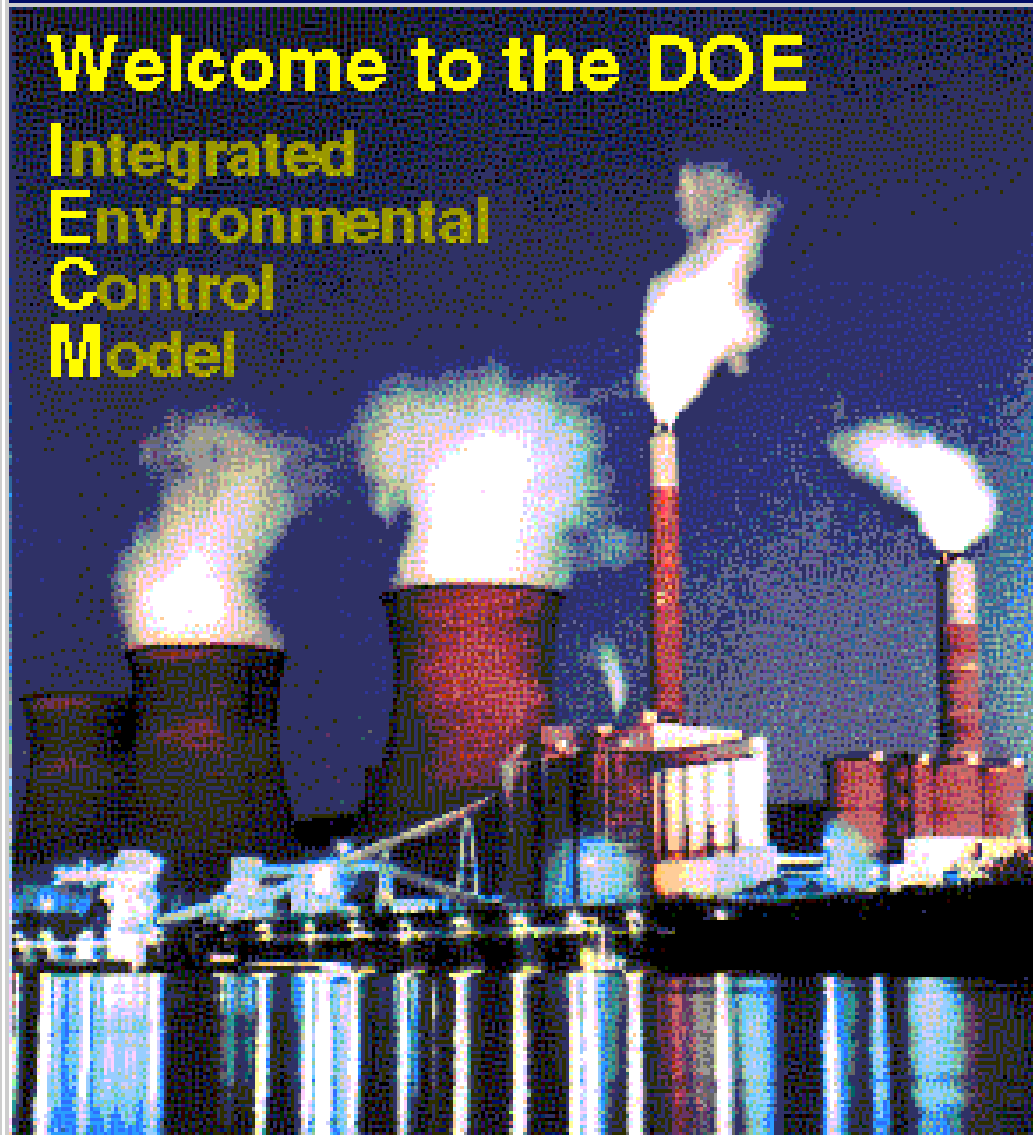
- ABB Power Plant Control
- American Electric Power
- Consol, Inc.
- Energy & Env. Research Corp.
- Exportech Company, Inc.
- FirstEnergy Corp.
- FLS Miljo A/S
- Foster Wheeler Development Corp.
- Lehigh University
- Lower Colorado River Authority
- McDermott Technology, Inc.
- Mitsui Babcock Energy LTD.
- National Power Plc.
- Niksa Energy Associates
- Pacific Corp.
- Pennsylvania Electric Association
- Potomac Electric Power Co.
- Savvy Engineering
- Sierra Pacific Power Co.
- Southern Company Services, Inc.
- Stone & Webster Engineering Corp.
- Tampa Electric Co.
- University of California, Berkeley
- US Environmental Protection Agency



About the IECM Interface



# Welcome to the DOE Integrated Environmental Control Model



IECM 3.3 B © 2000, Carnegie Mellon University

IECM Interface 3.3 B © 2000, Carnegie Mellon University

## Example

**Configure Plant****Set Parameters****Get Results****Combustion Controls**

Furnace Type: Tangential

NOx Control: Low NOx Burners

**Post-Combustion Controls**

NOx Control: None

Particulates: None

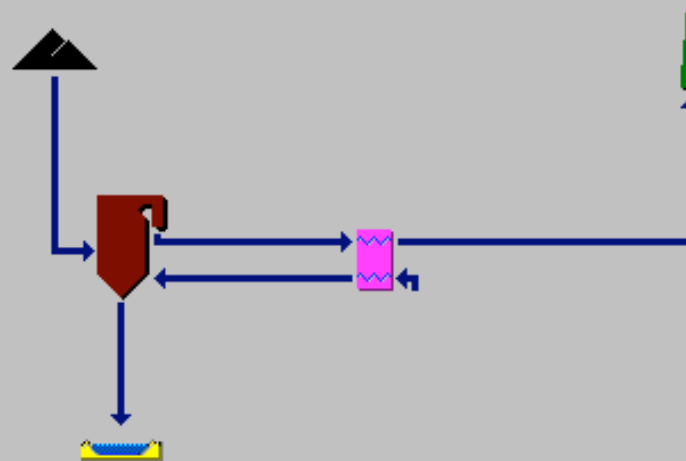
SO2 Control: None

SO2/NOx: None

**Solids Management**

Recovery: None

Fly Ash Disposal: mixed w/ Landfill

**Plant Diagram**

**Configure Plant****Set Parameters****Get Results****Combustion Controls**

Furnace Type: Tangential

NOx Control: Low NOx Burners

**Post-Combustion Controls**

NOx Control: Hot-Side SCR

Particulates: None

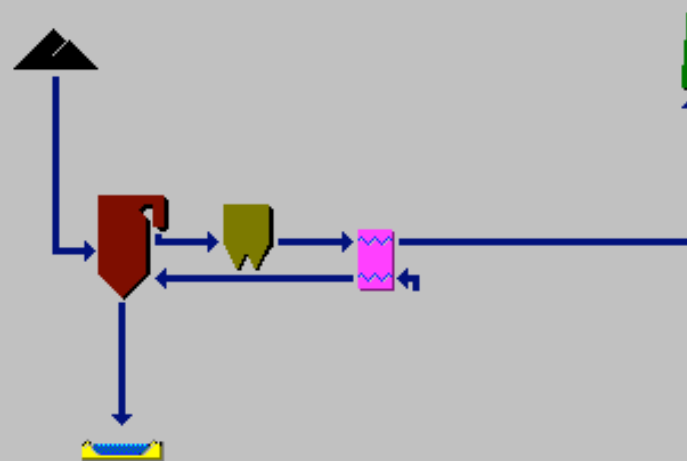
SO2 Control: None

SO2/NOx: None

**Solids Management**

Recovery: None

Fly Ash Disposal: mixed w/ Landfill

**Plant Diagram**

## Example

Configure PlantSet ParametersGet ResultsCombustion Controls

Furnace Type: Tangential

NOx Control: Low NOx Burners

Post-Combustion Controls

NOx Control: Hot-Side SCR

Particulates: Cold-Side ESP

SO2 Control: None

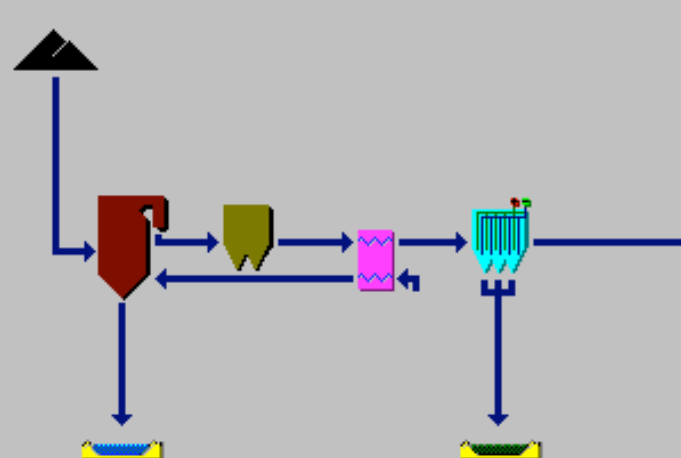
SO2/NOx: None

Solids Management

Recovery: None

Fly Ash Disposal: mixed w/ Landfill

## Plant Diagram



**Configure Plant****Set Parameters****Get Results****Combustion Controls**

Furnace Type: Tangential

NOx Control: Low NOx Burners

**Post-Combustion Controls**

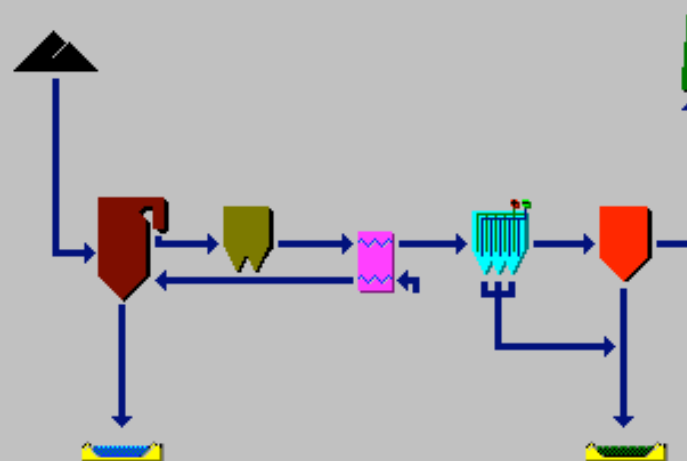
NOx Control: Hot-Side SCR

Particulates: Cold-Side ESP

SO<sub>2</sub> Control: Wet FGDSO<sub>2</sub>/NO<sub>x</sub>: None**Solids Management**

Recovery: None

Fly Ash Disposal: mixed w/ Landfill

**Plant Diagram**

IECM Interface

FileEditViewWindowHelp

Untitled

Configure PlantSet ParametersGet Results

Combustion Controls

Furnace Type:

Tangential

NOx Control:

Low NOx Burners

Post-Combustion Controls

NOx Control:

Hot-Side SCR

Particulates:

Cold-Side ESP

SO2 Control:

Wet FGD

SO2/NOx:

None

CO2 Control:

Absorption - MEA

By-Product Management

Recovery:

None

Fly Ash Disposal:

mixed w/ Landfill

CO2 Storage:

Depleted Oil Wells

Plant Diagram

Plant Diagram

Depleted Oil Wells

## Example

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantCoal  
PropertiesBase  
PlantFurnace  
FactorsEmission  
ConstraintsNOx  
ControlParticulate  
ControlSO<sub>2</sub> ControlSolid Waste  
Mgmt

## Current Coal

Name: Appalachian Medium Sulfur

Rank: Bituminous

Source: Model Default Coals

Composition (wt% as fired) and  
Higher Heating Value (Btu/lb)

	Property	Value
1	Heating Value	1.326e+04
2	Carbon	73.81
3	Hydrogen	4.880
4	Oxygen	5.410
5	Chlorine	7.000e-02
6	Sulfur	2.130
7	Nitrogen	1.420
8	Ash	7.230
9	Moisture	5.050
10	Cost (\$/ton)	32.07
11		

Save As  
User-DefinedAdd to  
FavoritesUse Default  
Ash PropertiesEdit Ash  
Properties

## Favorite Coals

Name: Wyoming Powder River Basin

Rank: Sub-Bituminous

Wyoming Powder River Basin

	Property	Value
1	Heating Value	8340
2	Carbon	48.18
3	Hydrogen	3.310
4	Oxygen	11.87
5	Chlorine	1.000e-02
6	Sulfur	0.3700
7	Nitrogen	0.7000
8	Ash	5.320
9	Moisture	30.24
10	Cost (\$/ton)	12.46
11		

Browse All  
CoalsUse This  
CoalRemove From  
FavoritesView Ash  
Properties

1. Coal Prop.

2. Cost

## IECM Interface

File Edit View Window Help

## Example

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantCoal  
PropertiesBase  
PlantFurnace  
FactorsEmission  
ConstraintsNOx  
ControlParticulate  
ControlSO<sub>2</sub> ControlSolid Waste  
Mgmt

	Title	Units	Unc	Value	Calc	Min	Max	Default
1	Gross Electrical Output	MWg		500		1	3000	500
2	Steam Cycle Heat Rate	Btu/kWh		7880		6000	11000	7880
3	Boiler Efficiency	%		89.21	<input checked="" type="checkbox"/>	0	100	calc
4	Capacity Factor	%		75		0	100	75
5	Excess Air For Furnace	% stoich.		20.00	<input checked="" type="checkbox"/>	0	40	calc
6	Leakage Air at Preheater	% stoich.		19.00	<input checked="" type="checkbox"/>	0	60	calc
7	Gas Temp. Exiting Economizer	deg. F		700		250	1200	700
8	Gas Temp. Exiting Air Preheater	deg. F		300		150	400	300
9	Ambient Air Temperature	deg. F		80		-50	130	80
10	Ambient Air Pressure	psia		14.7		12	15	14.7
11	Ambient Air Humidity	lb H <sub>2</sub> O/lb dry air		0.018		0	0.03	0.018
12	Collected Bottom Ash Solids	%		60.70	<input checked="" type="checkbox"/>	0	100	calc
13	Base Plant Energy Requirements							
14	Coal Pulverizer	% MWg		0.6000	<input checked="" type="checkbox"/>	0	2	calc
15	Steam Cycle Pumps	% MWg		0.65		0	2	0.65
16	Forced Draft Fans	% MWg		1.5		0	4	1.5
17	Cooling System	% MWg		1.8		0	2	1.8
18	Miscellaneous	% MWg		1.3		0	4	1.3

1. Performance

2. Financing

3. Retrofit Cost

4. Capital Cost

5. O&amp;M Cost

6. O&amp;M Escalation



**Uncertainty Editor**

Plant Parameter	Units	Value	Minimum	Maximum
Maximum SO2 Removal Efficiency	%	95	90	99

**Distribution:** Triangular

Normalized: Min 0.9000 Mode 1.000 Max 1.023

Nominal: Min 85.50 Mode 95.00 Max 97.18

**Description:**

Triangular(a,b,c) describes a triangular-shaped distribution where the values a, b, and c represent the minimum, most likely and maximum values, respectively.

**Uncertainty Tools: Untitled**

Uncertainty Areas

☒ Base Plant ☒ NOx Control

☒ Air Preheater ☒ Particulate Control

☒ Solid Waste Mgmt. ☒ SO2 Control

☒ SO2/NOx Control

Select All Select None

Sample Size: 50

Sampling Method: Median LHS

## Example

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantFuel  
(Coal)

Boiler

Air  
PreheaterNO<sub>x</sub>  
ControlParticulate  
ControlSO<sub>2</sub>  
Control

Pond

Landfill

Stack

	Stack Gas Component	Flow Rate (ton/hr)
1	N <sub>2</sub>	1771
2	O <sub>2</sub>	149.0
3	H <sub>2</sub> O	252.7
4	CO <sub>2</sub>	454.3
5	CO	0.0
6	HCl	2.395e-02
7	SO <sub>2</sub>	1.300
8	SO <sub>3</sub>	3.137e-02
9	NO	0.2053
10	NO <sub>2</sub>	1.656e-02
11	Ash	3.313e-02
12	Total	2629
13		
14	SO <sub>x</sub>	1.331
15	NO <sub>x</sub>	0.2218

	Overall Flow Component	Flow Rate (ton/hr)
1	Coal	166.5
2	Lime/Limestone	9.729
3	Ammonia	0.3460
4	Total	176.6
5		
6	Bottom Ash	3.997
7	Fly Ash	9.638
8	FGD Waste	17.82
9	By-Product Ash	0.0
10	By-Product Gypsum	0.0
11	By-Product Sulfur	0.0
12	By-Product Acid	0.0
13	Total	31.45
14		
15		

1. Diagram

2. Perf. Summary

3. Flow Summary

4. Cost Summary

## Example

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantFuel  
(Coal)

Boiler

Air  
PreheaterNO<sub>x</sub>  
ControlParticulate  
ControlSO<sub>2</sub>  
Control

Pond

Landfill

Stack

	Technology	Capital Cost (M\$)	Capital Cost (\$/kW)	O&M Cost (M\$/yr)	Revenue Required (M\$/yr)	Revenue Required (mills/kWh)
1	NO <sub>x</sub> Control	24.04	52.97	3.160	5.645	1.892
2	TSP Control	19.67	43.34	1.739	3.565	1.194
3	SO <sub>2</sub> Control	64.13	141.3	10.13	17.66	5.917
4	Comb. SO <sub>x</sub> /NO <sub>x</sub>	0.0	0.0	0.0	0.0	0.0
5	Subtotal	107.8	237.6	15.03	26.87	9.003
6	Base Plant	437.7	964.2	58.29	99.73	34.69
7	Total	545.5	1202	73.32	126.6	43.70
8						
9						
10						
11						
12						
13						
14						
15						

Costs are in Constant 1996 dollars.

1. Diagram

2. Perf. Summary

3. Flow Summary

4. Cost Summary

## IECM Interface

File Edit View Window Help

## Example

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantFuel  
(Coal)

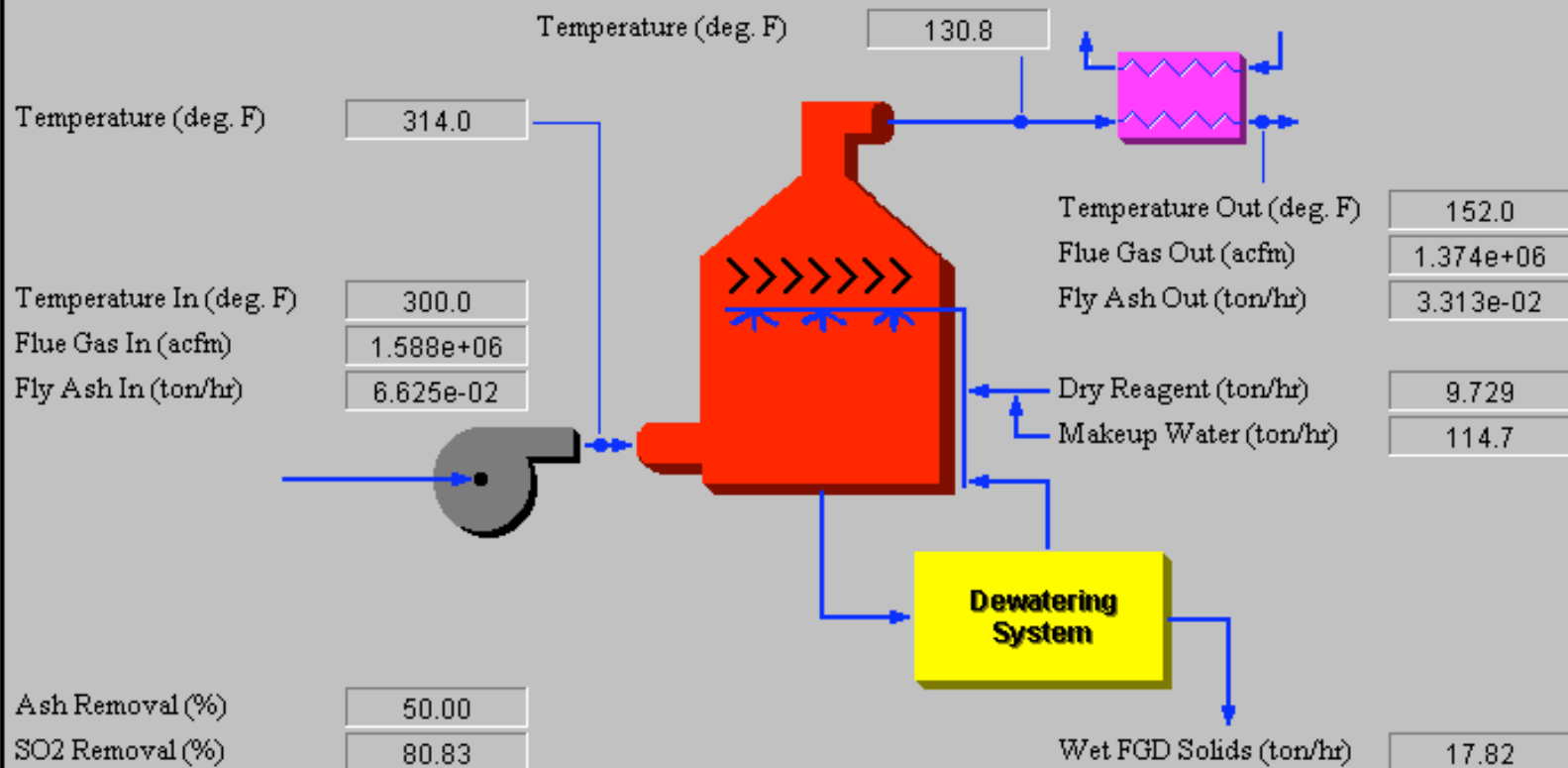
Boiler

Air  
PreheaterNOx  
ControlParticulate  
ControlSO<sub>2</sub>  
Control

Pond

Landfill

Stack



1. Diagram

2. Capital Cost

3. O&amp;M Cost

## Configure Plant

## Set Parameters

## Get Results

Overall  
PlantFuel  
(Coal)

Boiler

Air  
PreheaterNOx  
ControlParticulate  
ControlSO<sub>2</sub>  
Control

Pond

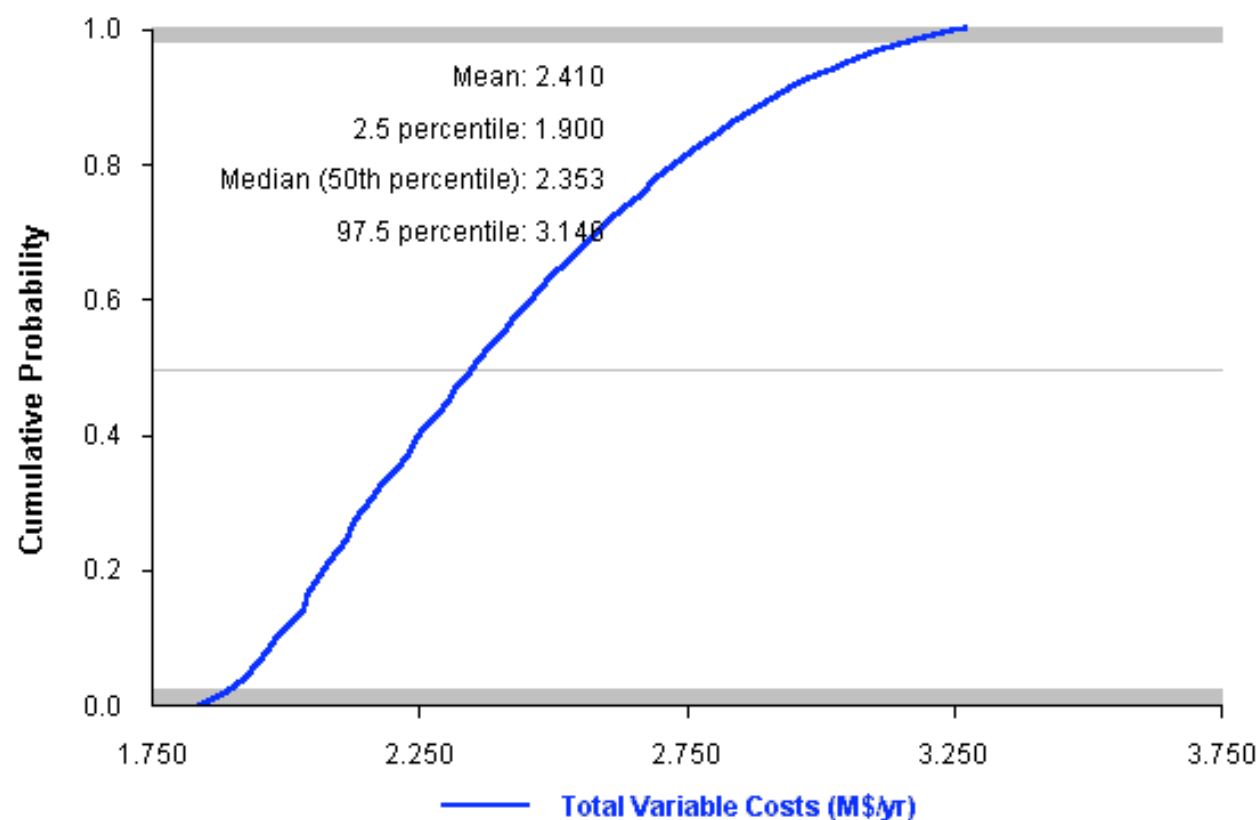
Landfill

Stack

Vari

1	Catalyst
2	Ammonia
3	Steam
4	Water
5	Power
6	Total Variable
7	
8	
9	
10	
11	
12	
13	
14	
15	

Example: CDF Graph of Total Variable Costs (M\$/yr)

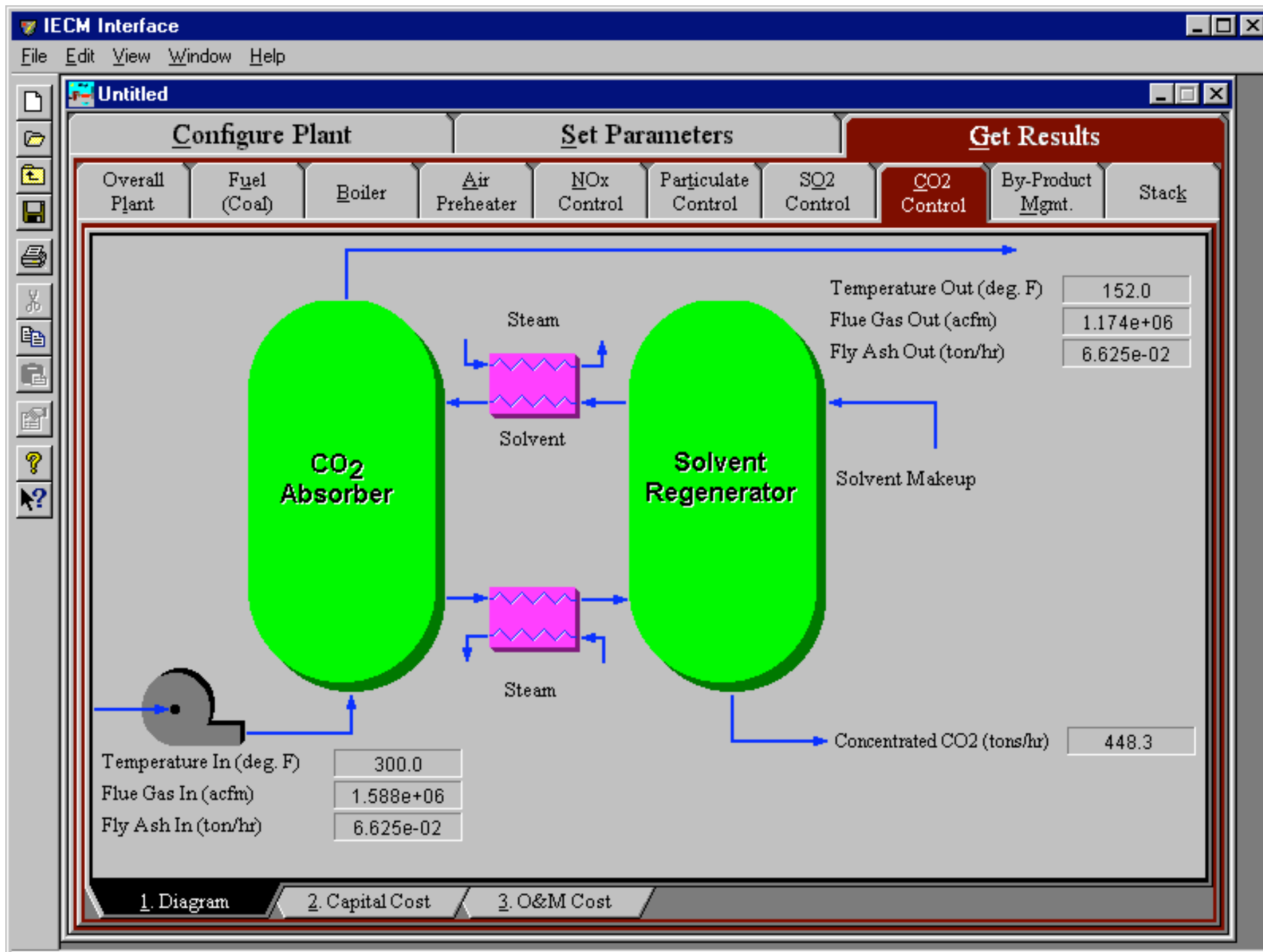


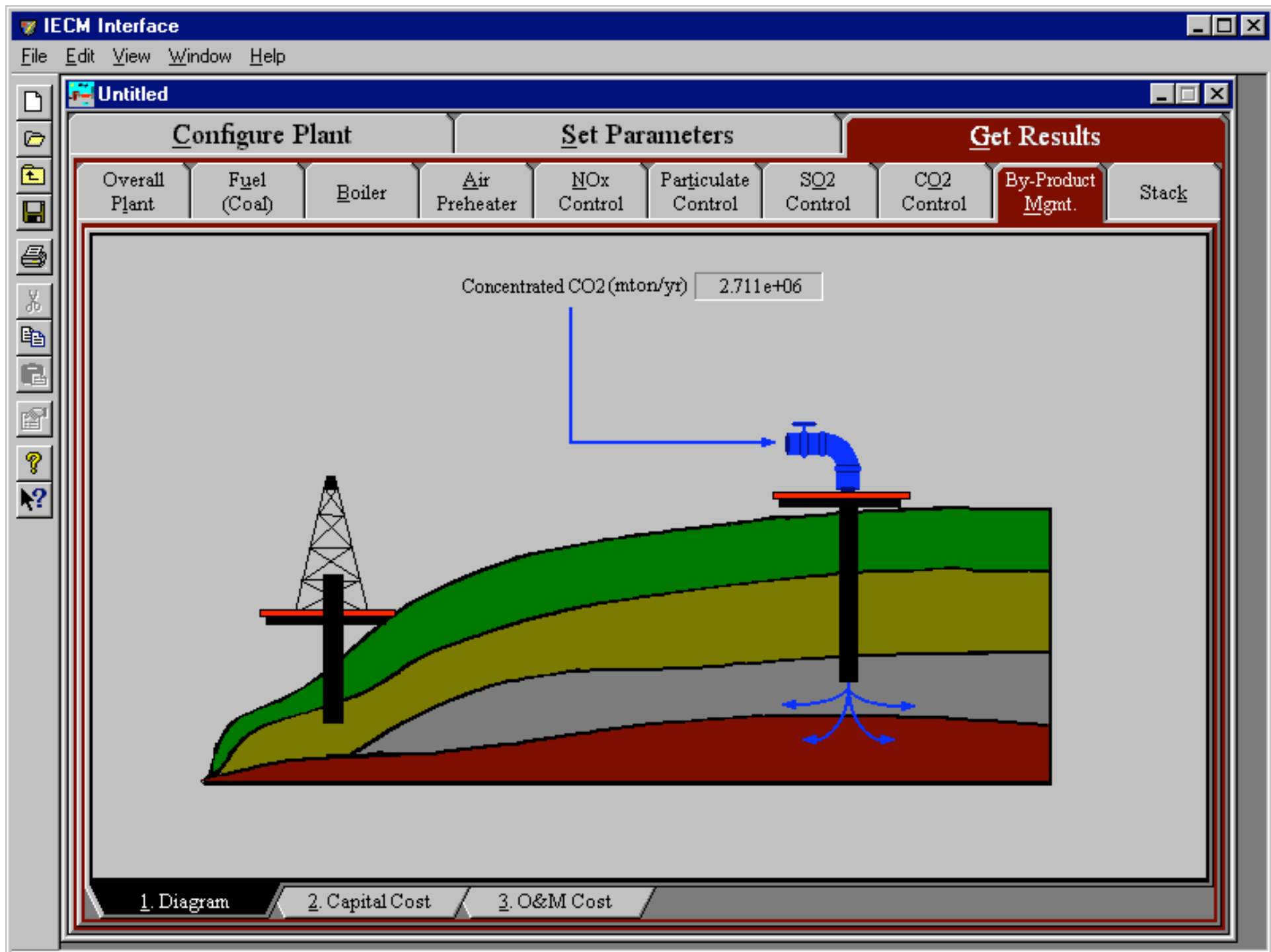
95% confidence interval between shaded areas

1. Diagram

2. Capital Cost

3. O&amp;M Cost





# CO<sub>2</sub> Module Results

- Flue gas (out) composition
- CO<sub>2</sub> emission level (kg CO<sub>2</sub>/hr)
- Amount of CO<sub>2</sub> product (ton/hr)
- Purity of CO<sub>2</sub> product (%)
- Solvent circulation rate (m<sup>3</sup>/hr)
- Make-up solvent rate (kg MEA/hr)
- Make-up rate relative to the circulation rate (%)
- Waste generation rate (kg/hr)
- Energy penalty (% of MW<sub>g</sub>)
- Net power generation
- Cost of CO<sub>2</sub> captured (\$/ tonCO<sub>2</sub> captured)
- Cost increase in electricity (cents/kWh)
- Cost of CO<sub>2</sub> avoided (\$/ tonCO<sub>2</sub> avoided)



# Additional Technology Options

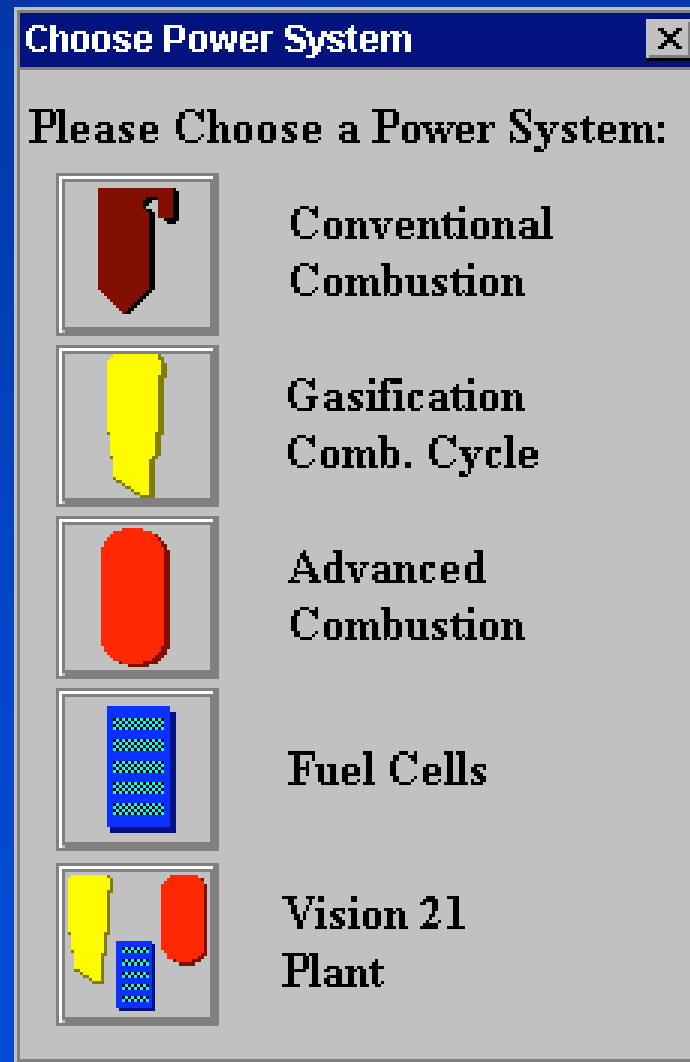
## ● *Just Completed*

- Combustion NO<sub>x</sub> Controls
  - Selective Non-Catalytic Reduction (SNCR)
  - Low NO<sub>x</sub> Burners (LNB)
  - LNB + Overfire air
  - LNB + SNCR
  - Natural Gas Reburn
  - Tangential, Wall & Cyclone Firing

## ● *Just Started*

- Post-Combustion Controls
  - Air Toxics (mercury)
- Other Fossil Fuels
- Alternative Power Generation Systems
- CO<sub>2</sub> Sequestration Options

# Future Developments: A Menu of Technology Options




# Select Gasification Combined Cycle (IGCC) Options




Choose Power System


Please Choose a Power System:




Conventional Combustion



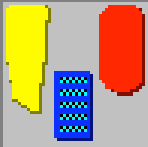
Gasification Comb. Cycle



Advanced Combustion

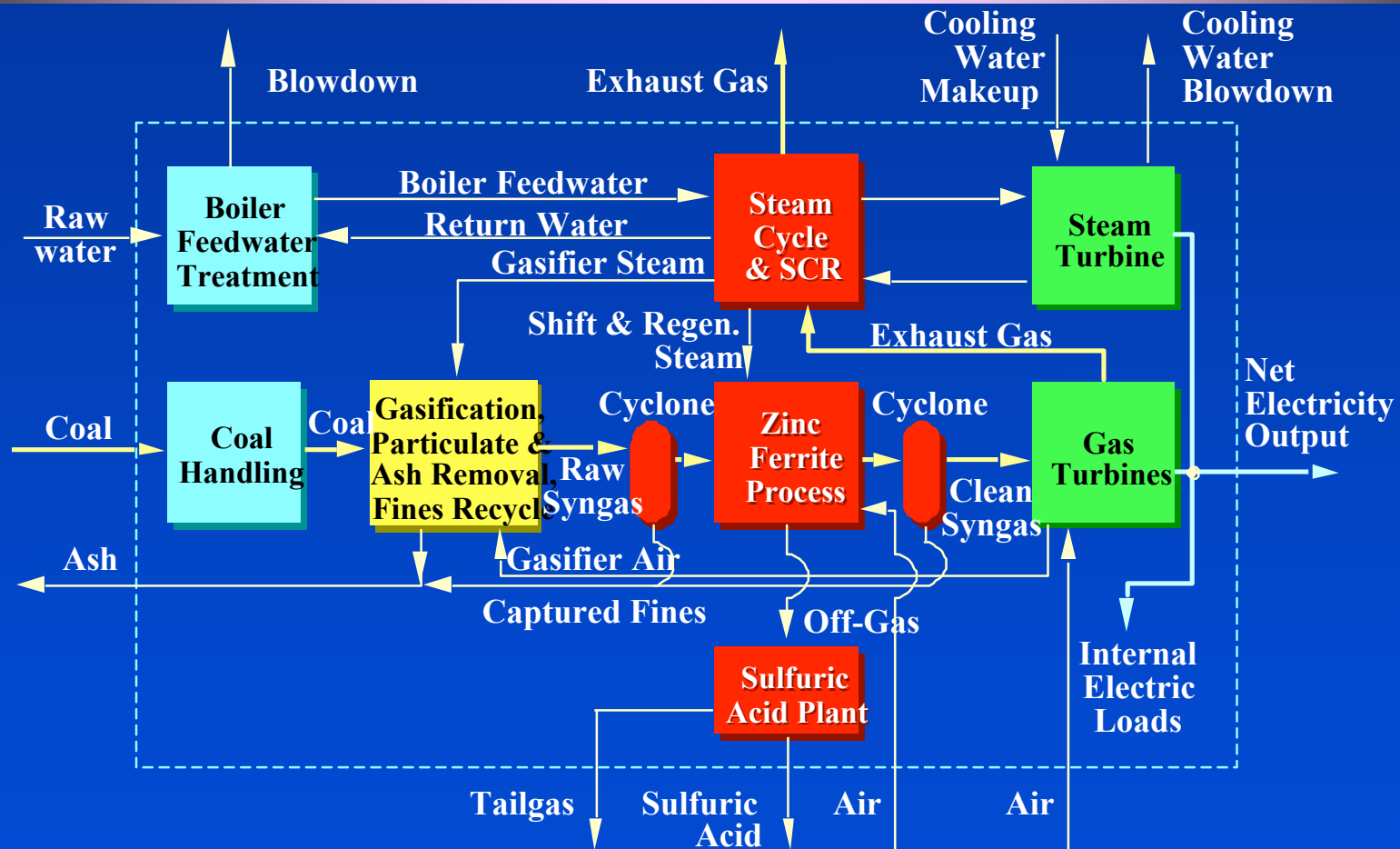


Fuel Cells

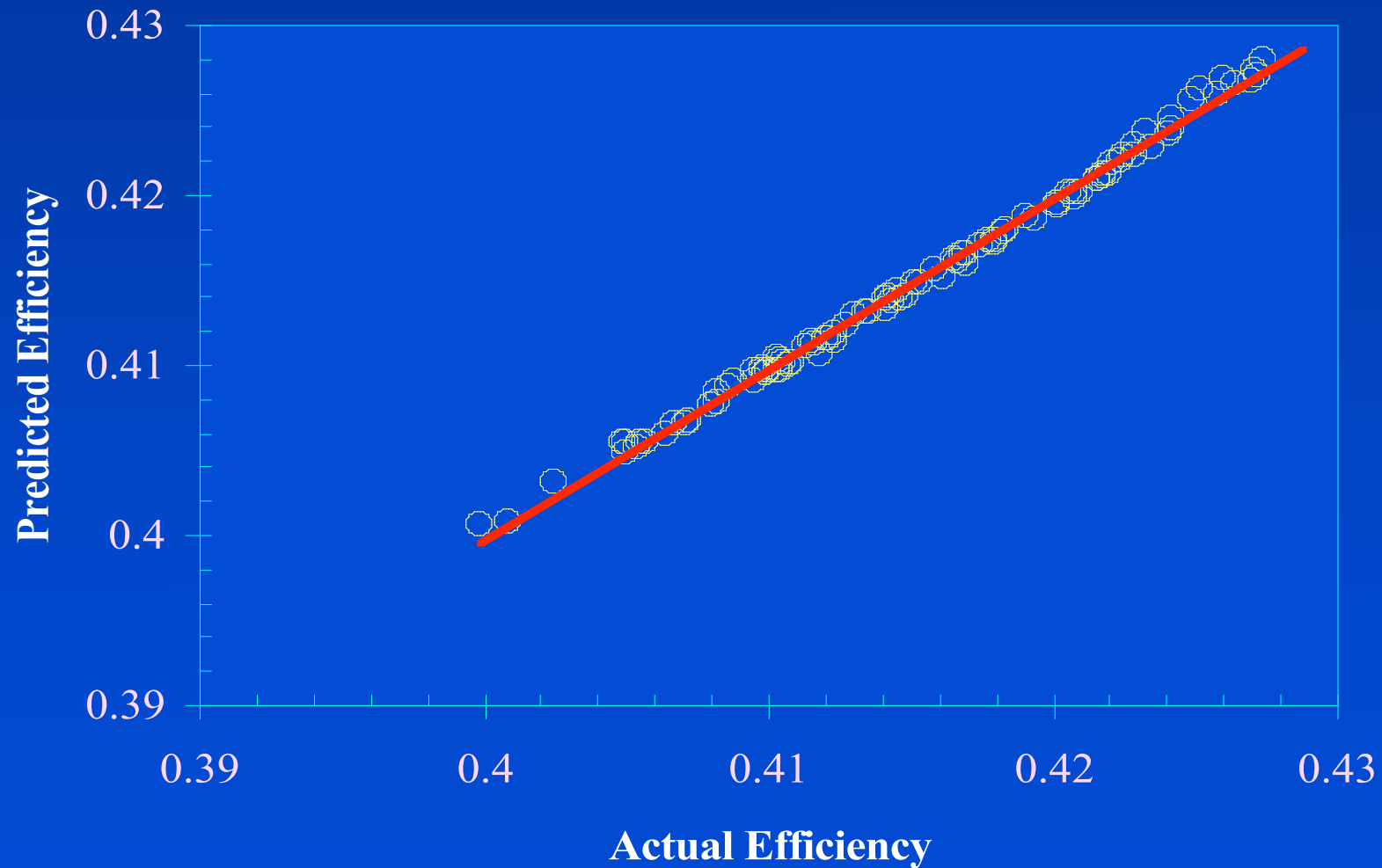


Vision 21 Plant

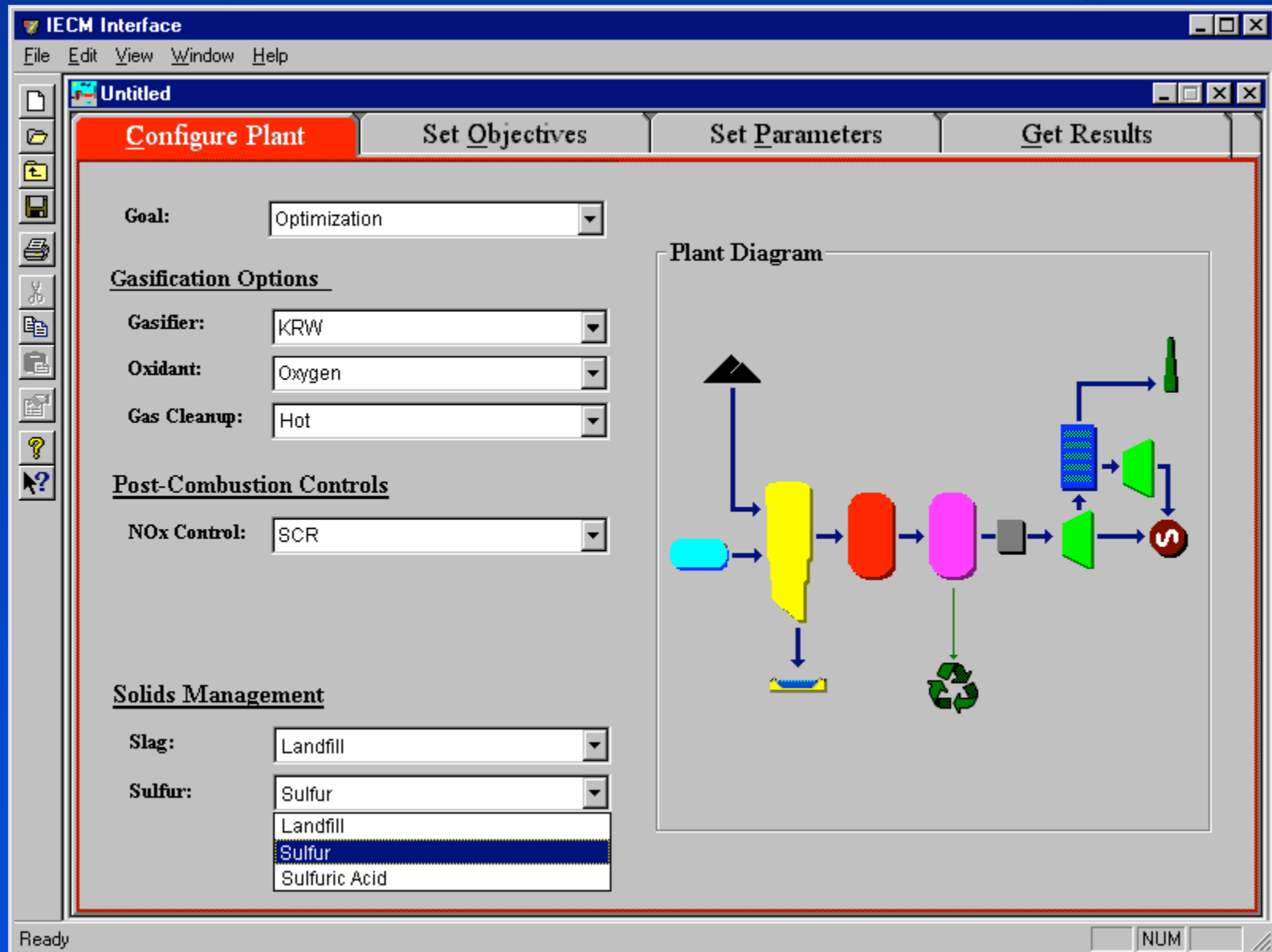
# ASPEN Model of an IGCC System



# Response Surface Model for an IGCC System



# Desktop Model of an IGCC System



# Model Applications

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- Process design
- Technology evaluation
- Cost estimation
- R&D management
- Risk analysis
- Environmental compliance
- Marketing studies
- Strategic planning

# A Hierarchy of Process Models

